

PATENT
2039.017800/RFE
PI210405

APPLICATION FOR UNITED STATES LETTERS PATENT

for

**MONOVINYLAARENE/CONJUGATED DIENE COPOLYMERS HAVING
LOWER GLASS TRANSITION TEMPERATURES**

by

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EXPRESS MAIL MAILING LABEL

NUMBER: EV 291397253 US

DATE OF DEPOSIT: NOVEMBER 10, 2003

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BACKGROUND OF THE INVENTION

The present invention relates generally to the fields of polymer chemistry. More particularly, it concerns monovinylarene- conjugated diene copolymers with lower T_g relative to reference styrene-butadiene copolymers.

Articles formed from monovinylarene-conjugated diene copolymers, such as styrene-butadiene copolymers, for example K-Resin® (Chevron Phillips Chemical Co., The Woodlands, TX), generally have a number of good physical properties. However, in the case of articles for which heat shrink is a desirable processing step, monovinylarene-conjugated diene copolymers are generally slightly less favorable for use, as their glass transition temperatures (T_g), which is the temperature at which shrinking occurs, are typically in the range of about 95°C to about 108°C. This relatively high T_g requires the use of a relatively large amount of heat to reach the temperatures at which shrinking occurs.

Therefore, it would be desirable to have monovinylarene-butadiene copolymers with lower T_g and more ready heat shrink processibility.

SUMMARY OF THE INVENTION

In one embodiment, the present invention relates to a monovinylarene/conjugated diene block copolymer, comprising:

a random (conjugated diene_x/monovinylarene_y)_m block, wherein x is about 2.5 wt% to about 10 wt%, y is from about 90 wt% to about 97.5 wt%, and x + y is about 97.5 wt% to 100 wt%; and

a (conjugated diene)_n block;
wherein n is from about 20 wt% to about 30 wt%, m is from about 70 wt% to about 80 wt%, and m + n is from about 90 wt% to 100 wt%.

In another embodiment, the present invention relates to an article, comprising the monovinylarene/conjugated diene block copolymer described above.

In a further embodiment, the present invention relates to a method of preparing a monovinylarene/conjugated diene block copolymer having a low T_g , comprising:

(a) charging a monovinylarene monomer, a conjugated diene monomer, an initiator, and a randomizer, allowing polymerizing to occur, to produce a random (conjugated diene_x/monovinylarene_y)_m block;

(b) charging a monovinylarene monomer, a conjugated diene monomer, and an initiator, allowing polymerization to occur, to produce a monovinylarene/conjugated diene block;

(c) charging a conjugated diene monomer, and allowing polymerization to occur, to produce a (conjugated diene)_n block; and

(c) charging the reaction mixture with a coupling agent, to form monovinylarene/conjugated diene block copolymer.

In yet another embodiment, the present invention relates to a method of fabricating an article, comprising:

forming a monovinylarene/conjugated diene block copolymer into the article, wherein the monovinylarene/conjugated diene block copolymer is as described above.

The present invention provides monovinylarene-conjugated diene copolymers with lower T_g and more ready heat shrink processibility.

BRIEF DESCRIPTION OF THE DRAWINGS

The following drawings form part of the present specification and are included to further demonstrate certain aspects of the present invention. The invention may be better understood by reference to one or more of these drawings in combination with the detailed description of specific embodiments presented herein.

Figure 1 shows the results of a differential scanning calorimetry (DSC) run of the polymer of Example 1.

Figure 2 shows the results of a DSC run of the polymer of Example 2.

Figure 3 shows the results of a DSC run of the polymer of Comparative Example 5, a reference polymer to the polymers of Examples 1-2.

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DESCRIPTION OF ILLUSTRATIVE EMBODIMENTS

In one embodiment, the present invention relates to a monovinylarene/conjugated diene block copolymer, comprising:

10 a random (conjugated diene_x/monovinylarene_y)_m block, wherein x is about 2.5 wt% to about 10 wt%, y is from about 90 wt% to about 97.5 wt%, and x + y is about 97.5 wt% to 100 wt%; and

a (conjugated diene)_n block;

wherein n is from about 20 wt% to about 30 wt%, m is from about 70 wt% to about 80 wt%, and m + n is from about 90 wt% to 100 wt%.

15 The basic starting materials and polymerization conditions for preparing conjugated diene/monovinylarene block copolymers are disclosed in U.S. Pat. Nos. 4,091,053; 4,584,346; 4,704,434; 4,704,435; and 5,227,419; the disclosures of which are hereby incorporated by reference.

20 "Conjugated diene," as used herein, refers to an organic compound containing conjugated carbon-carbon double bonds and a total of 4 to 12 carbon atoms, such as 4 to 8 carbon atoms. Exemplary conjugated dienes include, but are not limited to, 1,3-butadiene, 2-methyl-1,3-butadiene, 2-ethyl-1,3-butadiene, 2,3-dimethyl-1,3-butadiene, 1,3-pentadiene, 3-butyl-1,3-octadiene, and mixtures thereof. In one embodiment, the conjugated diene can be 1,3-butadiene or isoprene. In a further embodiment, the
25 conjugated diene can be 1,3-butadiene. A unit of a polymer, wherein the unit is derived from polymerization of a conjugate diene monomer, is a "conjugated diene unit."

"Monovinylarene," as used herein, refers to an organic compound containing a single carbon-carbon double bond, at least one aromatic moiety, and a total of 8 to 18 carbon atoms, such as 8 to 12 carbon atoms. Exemplary monovinylarenes include, but
30 are not limited to, styrene, alpha-methylstyrene, 2-methylstyrene, 3-methylstyrene, 4-

methystyrene, 2-ethylstyrene, 3-ethylstyrene, 4-ethylstyrene, 4-n-propylstyrene, 4-t-butylstyrene, 2,4-dimethylstyrene, 4-cyclohexylstyrene, 4-decylstyrene, 2-ethyl-4-benzylstyrene, 4-(4-phenyl-n-butyl)styrene, 1-vinylnaphthalene, 2-vinylnaphthalene, and mixtures thereof. In one embodiment, the monovinylarene is styrene. A unit of a polymer, wherein the unit is derived from polymerization of a monovinylarene monomer, is a “monovinylarene unit.”

In the polymer of the present invention, the random (conjugated diene_x/monovinylarene_y)_m block comprises conjugated diene units and monovinylarene units. The block is “random” in that the probability of any particular unit being a conjugated diene unit or a monovinylarene unit is substantially the same as the mole fractions of conjugated diene and monovinylarene in the block. This does not preclude the possibility of short stretches of the block having regularity (*i.e.*, appearing non-random), but such regular stretches will typically be present at no more than about the level expected by chance.

In the random (conjugated diene_x/monovinylarene_y)_m block, the conjugated diene units can be present at a weight fraction *x*, wherein *x* can be about 2.5 wt% to about 10 wt%, and the monovinylarene units can be present at a weight fraction *y*, wherein *y* can be from about 90 wt% to about 97.5 wt%.

In one embodiment, *x* can be about 5 wt% to about 10 wt%.

In one embodiment, *y* can be about 90 wt% to about 95 wt%.

As will be apparent to the skilled artisan, *x* + *y* can be less than or equal to 100 wt%. In one embodiment, *x* + *y* can be about 97.5 wt% to 100 wt%.

In the event that *x* + *y* is less than 100 wt%, the balance of the weight fraction of the random (conjugated diene_x/monovinylarene_y)_m block can comprise one or more other units. Any other units that are capable of inclusion in a polymer by vinyl addition polymerization can be the other units providing the balance of the weight fraction of the random (conjugated diene_x/monovinylarene_y)_m block.

The (conjugated diene)_n block comprises conjugated diene units, and can also comprise a small amount (less than about 1 wt%) of one or more other units. Any other

units that are capable of inclusion in a polymer by vinyl addition polymerization can be the other units comprising the small amount of the (conjugated diene)_n block.

The proportions of the random (conjugated diene_x/monovinylarene_y)_m block and the (conjugated diene)_n block can be defined by their weight fractions, m and n.

5 In one embodiment, n can be from about 5 wt% to about 45 wt% and m can be from about 55 wt% to about 95 wt%. In a further embodiment, n can be from about 20 wt% to about 30 wt% and m can be from about 70 wt% to about 80 wt%. In another embodiment, n can be about 25 wt% and m can be about 75 wt%.

10 As will be apparent to the skilled artisan, m + n can be less than or equal to 100 wt%. In one embodiment, m + n can be from about 90 wt% to 100 wt%.

In the event that m + n is less than 100 wt%, the balance of the weight fraction of the copolymer can comprise one or more other blocks. Any other blocks that are capable of inclusion in a block copolymer by vinyl addition polymerization can be the other blocks providing the balance of the weight fraction of the copolymer. An example of
15 such a block is, but is not limited to, a polymonovinylarene block.

The inventive polymer contains at least one random (conjugated diene_x/monovinylarene_y)_m block and at least one (conjugated diene)_n block. The blocks can be incorporated sequentially into the polymer in any order. The inventive polymer can contain more than one random (conjugated diene_x/monovinylarene_y)_m block, more
20 than one (conjugated diene)_n block, or both. If a plurality of either or both type of block is present, the blocks can be incorporated sequentially into the polymer in any order (e.g., alternating between the random block and the conjugated diene block, or present in a sequence of blocks of one type followed by a sequence of blocks of another type, among other incorporation sequences).

25 Generally, each block is formed by polymerizing the monomer or mixture of monomers from which the desired units of the block are derived. The polymerization process will generally be amenable to a relative lack of change in process parameters between different blocks, but the skilled artisan, having the benefit of the present disclosure, may make some minor changes in process parameters between different
30 blocks as a matter of routine experimentation. The following descriptions of the

polymerization process will generally apply to the formation of all types of blocks in the inventive polymer, although certain descriptions may be of more or less value to forming one or more of the types of blocks in the inventive polymer.

5 The polymerization process can be carried out in a hydrocarbon diluent at any suitable temperature in the range of from about -100°C to about 150°C, such as from about 0°C to about 150°C, and at a pressure sufficient to maintain the reaction mixture substantially in the liquid phase. In one embodiment, the hydrocarbon diluent can be a linear or cyclic paraffin, or mixtures thereof. Exemplary linear or cyclic paraffins include, but are not limited to, pentane, hexane, octane, cyclopentane, cyclohexane, and
10 mixtures thereof, among others. In one embodiment, the paraffin is cyclohexane.

The polymerization process can be carried out in the substantial absence of oxygen and water, such as under an inert gas atmosphere.

The polymerization process can be performed in the presence of an initiator. In one embodiment, the initiator can be any organomonoalkali metal compound known for
15 use as an initiator. In a further embodiment, the initiator can have the formula RM, wherein R is an alkyl, cycloalkyl, or aryl radical containing 4 to 8 carbon atoms, such as an n-butyl radical, and M is an alkali metal, such as lithium. In a particular embodiment, the initiator is n-butyl lithium.

The amount of initiator employed depends upon the desired polymer or block
20 molecular weight, as is known in the art and is readily determinable, making due allowance for traces of poisons in the feed streams. In one embodiment, the initiator can be present in an amount in the range of from about 0.01 phm (parts by weight per hundred parts by weight of total monomer) to about 1.0 phm. In another embodiment, the initiator can be present in an amount in the range of from about 0.01 phm to about 0.5
25 phm. In a further embodiment, the initiator can be present in an amount in the range of from about 0.01 phm to 0.2 phm.

The polymerization process can further involve the inclusion of small amounts of randomizers. In one embodiment, the randomizer can be a polar organic compound, such as an ether, a thioether, or a tertiary amine. In another embodiment, the randomizer can
30 be a potassium salt or a sodium salt of an alcohol. The randomizer can be included in the

hydrocarbon diluent to improve the effectiveness of the initiator, to randomize at least part of the monovinylarene monomer in a mixed monomer charge, or both. The inclusion of a randomizer can be of value when forming a random (conjugated diene_x/monovinylarene_y)_m block of the present polymer. Exemplary randomizers include, but are not limited to, dimethyl ether, diethyl ether, ethyl methyl ether, ethyl propyl ether, di-n-propyl ether, di-n-octyl ether, anisole, dioxane, 1,2-dimethoxyethane, dibenzyl ether, diphenyl ether, 1,2-dimethoxybenzene, tetramethylene oxide (tetrahydrofuran or THF), potassium tert-amylate (KTA), dimethyl sulfide, diethyl sulfide, di-n-propyl sulfide, di-n-butyl sulfide, methyl ethyl sulfide, dimethylethylamine, tri-n-ethylamine, tri-n-propylamine, tri-n-butylamine, trimethylaniline, triethylamine, tetramethylethylenediamine, tetraethylethylenediamine, N,N-di-methylaniline, N-methyl-N-ethylaniline, N-methylmorpholine, and mixtures thereof, among others.

In one embodiment, the randomizer is tetrahydrofuran. When employing tetrahydrofuran, the tetrahydrofuran is generally present in an amount in the range of from about 0.01 phm to about 1.0 phm, such as from about 0.02 phm to about 1.0 phm.

In another embodiment, the randomizer is potassium tert-amylate (KTA). When employing KTA, the KTA is generally present in an amount in the range of from about 0.01 phm to about 1.0 phm, such as from about 0.1 phm to about 1.0 phm.

When forming a particular block, each monomer charge or monomer mixture charge is polymerized under solution polymerization conditions such that the polymerization of each monomer charge or monomer mixture charge, to form the particular block, is substantially complete before charging a subsequent charge. "Charging," as used herein, refers to the introduction of a compound to a reaction zone, such as the interior of a reactor vessel.

A coupling agent can be added after polymerization is complete. Suitable coupling agents include, but are not limited to, di- or multivinylarene compounds; di- or multi epoxides; di- or multiisocyanates; di- or multiimines; di- or multialdehydes; di- or multiketones; alkoxytin compounds; di- or multihalides, such as silicon halides and halosilanes; mono-, di-, or multianhydrides; di- or multiesters, such as the esters of monoalcohols with polycarboxylic acids; diesters which are esters of monohydric

alcohols with dicarboxylic acids; diesters which are esters of monobasic acids with polyalcohols such as glycerol; and mixtures of two or more such compounds, among others.

Useful multifunctional coupling agents include, but are not limited to, epoxidized vegetable oils such as epoxidized soybean oil, epoxidized linseed oil, and mixtures thereof, among others. In one embodiment, the coupling agent is epoxidized soybean oil. Epoxidized vegetable oils are commercially available under the tradename Vikoflex® from Atofina Chemicals (Philadelphia, PA).

Any effective amount of the coupling agent can be employed. In one embodiment, a stoichiometric amount of the coupling agent relative to active polymer alkali metal tends to promote maximum coupling. However, more or less than stoichiometric amounts can be used for varying coupling efficiency where desired for particular products. Typically the total amount of coupling agent employed in the polymerization is in the range of from about 0.1 phm to about 20 phm, such as from about 0.1 phm to about 5 phm, or from about 0.1 phm to about 2 phm.

Following completion of the coupling reaction, the polymerization reaction mixture can be treated with a terminating agent such as water, alcohol, phenols, or linear saturated aliphatic mono-dicarboxylic acids, to remove alkali metal from the block copolymer and for color control. In one embodiment, the terminating agent is a mixture of water and carbon dioxide.

After termination, the polymer cement (polymer in polymerization solvent) usually contains about 10 to 40 weight percent solids, more usually 20 to 35 weight percent solids. The polymer cement can be flashed to evaporate a portion of the solvent so as to increase the solids content to a concentration of about 50 to about 99 weight percent solids, followed by vacuum oven or devolatilizing extruder drying to remove the remaining solvent.

The block copolymer can be recovered and worked into a desired shape, such as by milling, extrusion, or injection molding. The block copolymer can also contain additives such as antioxidants, antiblocking agents, release agents, fillers, extenders, and dyes, and the like.

In specific polymerization processes, typical initiator, monomer and monomer mixture charge sequences include, but are not limited, to the following.

Charging embodiment 1:

- 5 (a) randomizer, initiator, conjugated diene/monovinylarene monomer mixture
- (b) initiator, conjugated diene/monovinylarene monomer mixture
- (c) conjugated diene monomer
- (d) coupling agent

Charging embodiment 2:

- 10 (a) initiator, monovinylarene monomer
- (b) randomizer, initiator, conjugated diene/monovinylarene monomer mixture
- (c) conjugated diene monomer
- (d) randomizer, initiator, conjugated diene/monovinylarene monomer mixture
- 15 (e) conjugated diene monomer
- (f) coupling agent

In other embodiments, the monovinylarene/conjugated diene block copolymer of the present invention can comprise the following structures, wherein (B/S) is a random monovinylarene/conjugated diene block; <B/S> is a tapered monovinylarene/conjugated diene block; B is a conjugated diene block; S is a monovinylarene block; CA is a coupling agent residue; and - is a covalent linkage between blocks.

- (B/S)-(B/S)-B-CA
- (B/S)-B-CA
- 25 • (B/S)-(B/S)-B-(B/S)-B-CA
- (B/S)-B-(B/S)-B-CA
- S-(B/S)-B-(B/S)-B-CA
- <B/S>1-<B/S>2-<B/S>3-<B/S>4-<B/S>5-CA
- <B/S>2-<B/S>3-<B/S>4-<B/S>5-CA
- 30 • (B/S)1-(B/S)2-<B/S>3-<B/S>4-<B/S>5-CA

- (B/S)1-(B/S)2-(B/S)3-(B/S)4-(B/S)5-CA;

wherein $\langle B/S \rangle 1$, $\langle B/S \rangle 2$, (B/S)1, and (B/S)2 each have a conjugated diene content from about 2.5 wt% to about 10 wt%, and $\langle B/S \rangle 3$, $\langle B/S \rangle 4$, $\langle B/S \rangle 5$, (B/S)3, (B/S)4, and (B/S)5 each have a conjugated diene content from about 30 wt% to about 70 wt%.

A monovinylarene/conjugated diene block copolymer of the present invention can have a T_g of at least about 10°C less than the T_g of a reference polymer differing only in x being about 0 wt% and y being about 100 wt%.

T_g is the glass transition temperature of a polymer, *i.e.*, the temperature below which the polymer is in a relatively hard and brittle glass-like state, and above which the polymer is in a relatively soft and flexible plastic-like state. T_g can be measured by known techniques and apparatus, such as differential scanning calorimetry (DSC). Each polymer inherently has a glass transition temperature.

A reference polymer, as used herein, is a polymer identical to a monovinylarene/conjugated diene block copolymer of the present invention, in terms of the block identities and the values of m and n. The reference polymer differs only in x being about 0 wt% and y being about 100 wt% (*i.e.*, instead of a random (conjugated diene_x/monovinylarene_y)_m block, the reference polymer has a block that consists essentially of monovinylarene).

As stated above, in one embodiment, the monovinylarene/conjugated diene block copolymer of the present invention can have a T_g at least about 10°C less than the T_g of the reference polymer. In another embodiment, the monovinylarene/conjugated diene block copolymer can have a T_g at least about 20°C less than the T_g of the reference polymer. In a further embodiment, the monovinylarene/conjugated diene block copolymer can have a T_g at least about 30°C less than the T_g of the reference polymer.

Such lower T_g allows easier processing of monovinylarene/conjugated diene copolymers to form shrink films, among other articles.

In one embodiment, the present invention relates to an article, comprising the monovinylarene/conjugated diene block copolymer described above.

The article can be any article which can be fabricated, in whole or in part, from a monovinylarene/conjugated diene block copolymer known in the art, such as the
5 styrene/butadiene copolymer available under the tradename K-Resin® (Chevron Phillips Chemical Co., The Woodlands, TX).

Exemplary articles include, but are not limited to, containers, medical packaging, medical devices, toys, garment hangers, and flexible and rigid packaging, among others.

In one embodiment, the article is a shrink film, defined as a film that can shrink
10 upon exposure to temperatures of about 60°C to about 80°C.

In another embodiment, the present invention relates to a method of preparing a monovinylarene/conjugated diene block copolymer having a low T_g , comprising:

(a) charging a monovinylarene monomer, a conjugated diene monomer, an
15 initiator, and a randomizer, allowing polymerizing to occur, to produce a reaction mixture comprising a random (conjugated diene_x/monovinylarene_y)_m block;

(b) charging an initiator and a conjugated diene monomer, and allowing polymerization to occur, to produce a reaction mixture comprising a (conjugated diene)_n block; and

20 (c) charging the reaction mixture with a coupling agent, to form monovinylarene/conjugated diene block copolymer.

The charging steps (a)-(c) can be performed in accordance with the description set forth above. The proportions of the various components to be added in each of the charging steps is a matter of routine experimentation to the skilled artisan having benefit
25 of the present disclosure.

In one embodiment, the proportions of the components in charging step (a) can be chosen such that, in the product block, x is about 2.5 wt% to about 10 wt%, y is from about 90 wt% to about 97.5 wt%, and x + y is about 97.5 wt% to 100 wt%.

In one embodiment, the proportions of the components in charging steps (a) and
30 (b) can be chosen such that, in the product polymer, n is from about 20 wt% to about 30

wt%, m is from about 70 wt% to about 80 wt%, and m + n is from about 90 wt% to 100 wt%.

The sequence of steps (a) and (b) can be varied, and either or both of steps (a) and (b) can be performed one or more times.

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In another embodiment, the present invention relates to a method of fabricating an article, comprising:

forming a monovinylarene/conjugated diene block copolymer into the article, wherein the monovinylarene/conjugated diene block copolymer is as described above.

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The article can be any article referred to above.

In the forming step, the polymer can be formed into the article or a component thereof by any appropriate technique. Examples of appropriate techniques include, but are not limited to, sheet extrusion, thermoforming, injection molding, blow molding, film blowing, and film casting, among others. Selection of a forming technique is a matter of routine experimentation for the skilled artisan having the benefit of the present disclosure.

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The following examples are included to demonstrate particular embodiments of the invention. It should be appreciated by those of skill in the art that the techniques disclosed in the examples which follow represent techniques discovered by the inventor to function well in the practice of the invention. However, those of skill in the art should, in light of the present disclosure, appreciate that many changes can be made in the specific embodiments which are disclosed and still obtain a like or similar result without departing from the spirit and scope of the invention.

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Examples 1-2: Synthesis of random (conjugated diene_x/monovinylarene_y)_m/(conjugated diene)_n block copolymers

Two block copolymers were synthesized, as follows:

Example 1:

Compound charged	Amount charged (wt/vol units)	Time when Charged (min)	Reactor Temp (°C)
Cyclohexane	6.9 lbs	0.0	87.8
Tetrahydrofuran (THF)	4 cc (0.04 PHM)	2.7	40.3
Potassium <i>tert</i> - amylate (KTA)	5.6 cc (0.23 PHM)	2.8	41.6
<i>n</i> -butyl lithium	72.5 g (0.072 PHM)	3.0	43.0
butadiene/styrene mixture	50.1 g/690 g (2.5/34.5 PHM)	4.1	48.5
butadiene/styrene mixture	20.1 g/300.4 g (1.0/15.0 PHM)	16.2	62.9
<i>n</i> -butyl lithium	77.5 g (0.076 PHM)	30.3	62.4
butadiene/styrene mixture	30.2 g/411.7 g (1.5/20.5 PHM)	31.3	61.2
butadiene	500.8 g (25 PHM)	43.4	64.1
Vikoflex® (epoxidized soybean oil)	16.4 g (0.4 PHM)	61.4	86.9
H ₂ O	4.5 cc (0.2 PHM)	78.0	91.7
CO ₂	0.4 PHM	89.6	92.6
TNPP	0.5 PHM	112.1	93.5
Irganox 1010®	0.2 PHM	115.8	93.6

In addition to the above, each charge after the initial cyclohexane charge was followed with 0.2 lb cyclohexane (total cyclohexane at end of run was 9.0 lb).

Example 2:

Compound charged	Amount charged (wt/vol units)	Time when Charged (min)	Reactor Temp (°C)
Cyclohexane	6.9 lbs	0.0	65.7
THF	4 cc (0.04 PHM)	2.5	36.1
KTA	5.6 cc (0.23 PHM)	2.6	37.4
<i>n</i> -butyl lithium	73.1 g (0.072 PHM)	2.9	39.7
butadiene/styrene mixture	100.3 g/640.7 g (5/32 PHM)	3.9	44.1
butadiene/styrene mixture	40.2 g/280.2 g (2/14 PHM)	17.2	62.7
<i>n</i> -butyl lithium	77.9 g (0.076 PHM)	30.7	63.4
butadiene/styrene mixture	60.4 g/382.4 g (3/19 PHM)	32.0	61.9
butadiene	500.4 g (25 PHM)	44.1	65.6
Vikoflex®	17 g (0.4 PHM)	61.5	88.4
H ₂ O	4.5 cc (0.2 PHM)	78.1	91.7
CO ₂	0.4 PHM	89.2	92.4
TNPP	0.5 PHM	116.2	93.4
Irganox 1010®	0.2 PHM	118.5	93.4

In addition to the above, each charge after the initial cyclohexane charge was followed with 0.2 lb cyclohexane (total cyclohexane at end of run was 9.0 lb).

5 In both examples, at 5 min after the final charge, the contents of the reaction vessel were transferred to a blowdown vessel containing 3 g Be Square Wax (added before preheating of the blowdown vessel). The reactor and all lines were rinsed with 0.5 lb cyclohexane, and the rinse was transferred to the blowdown vessel. The blowdown vessel was then heated to 178°C, and the polymer was flashed to yield a polymer rope.

The polymer rope was dried in a vacuum oven (about 180°F to about 184°F) for 2.5 hr, chopped, and reserved for further study.

Comparative Example 3: Synthesis of Reference Polymer

Compound charged	Amount charged (wt/vol units)	Time when Charged (min)	Reactor Temp (°C)
Cyclohexane	6.9 lbs	0.0	97.3
THF	4 cc (0.04 PHM)	3.4	43.8
<i>n</i> -butyl lithium	85.3 g (0.085 PHM)	3.4	43.8
styrene	751.3 g (37.5 PHM)	6.4	45.0
styrene	321.2 g (16.0 PHM)	18.4	63.7
<i>n</i> -butyl lithium	69.8 g (0.07 PHM)	32.3	63.1
styrene	440.9 g (22 PHM)	36.0	61.2
butadiene	500.2 g (25 PHM)	48.0	62.4
Vikoflex®	16.0 g (0.4 PHM)	64.1	90.1
H ₂ O	4.5 cc (0.2 PHM)	83.2	95.4
CO ₂	0.2 PHM	93.2	96.4
TNPP	0.5 PHM	113.2	97.6
Irganox 1010®	0.2 PHM	113.2	97.6

5 In addition to the above, each charge after the initial cyclohexane charge was followed with 0.2 lb cyclohexane (total cyclohexane at end of run was 9.0 lb).

After the reaction, the polymer was retrieved and processed by the same procedure described for Examples 1-2, above.

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Examples 4-5 and Comparative Example 6: T_g of both random (conjugated diene_x/monovinylarene_y)_m/(conjugated diene)_n block copolymers and a reference polymer

Differential scanning calorimetry (DSC) was performed on the polymers generated in Examples 1-2, and a comparative reference polymer having styrene blocks

of essentially the same number and weight as the random butadiene/styrene blocks of the polymers of Examples 1-2. The T_g of each polymer was determined through standard techniques for analysis of heat flow vs. temperature graphs generated by DSC.

5 *Example 4*

The polymer of Example 1 was subjected to DSC. The results are shown in Figure 1. The T_g was 73.32°C.

10 *Example 5*

The polymer of Example 2 was subjected to DSC. The results are shown in Figure 2. The T_g was 63.96°C.

Comparative Example 6

15 The reference polymer of Comparative Examples 3 was subjected to DSC. The results are shown in Figure 3. The T_g was 95.50°C.

20 The results of Examples 4-5 and Comparative Example 6 indicate that the substitution of about 5-10 wt% butadiene into the styrene blocks of a butadiene/styrene block copolymer resulted in reductions in the T_g of at least about 10°C, such as about 20°C or 30°C, relative to the reference polymer.

25 All of the compositions and methods disclosed and claimed herein can be made and executed without undue experimentation in light of the present disclosure. While the compositions and methods of this invention have been described in terms of particular embodiments, it will be apparent to those of skill in the art that variations may be applied to the compositions and methods and in the steps or in the sequence of steps of the method described herein without departing from the concept, spirit and scope of the invention as defined by the appended claims.